

# A General Pressure Generation Model for Granular Propellant Fires

Frederick Paquet, Hoi Dick Ng and Mario Paquet



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# General background

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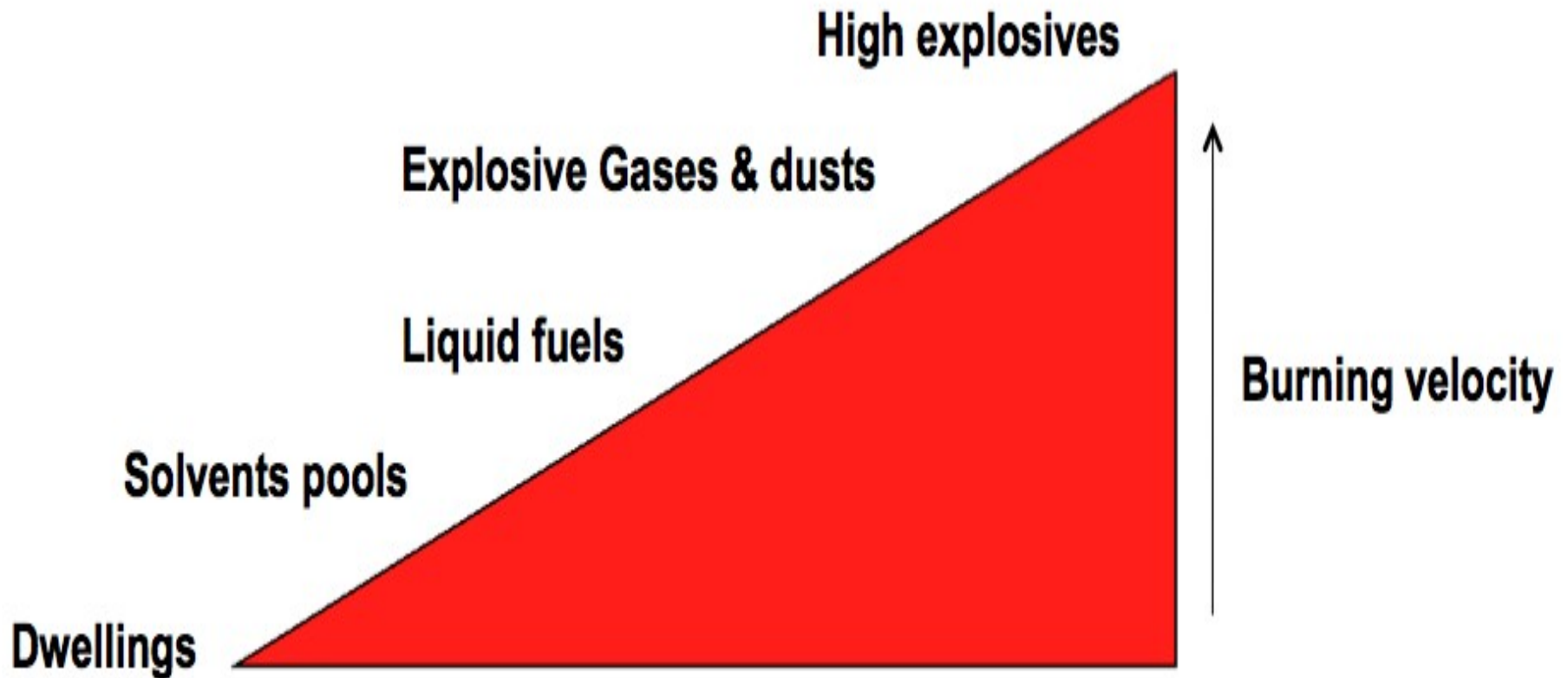
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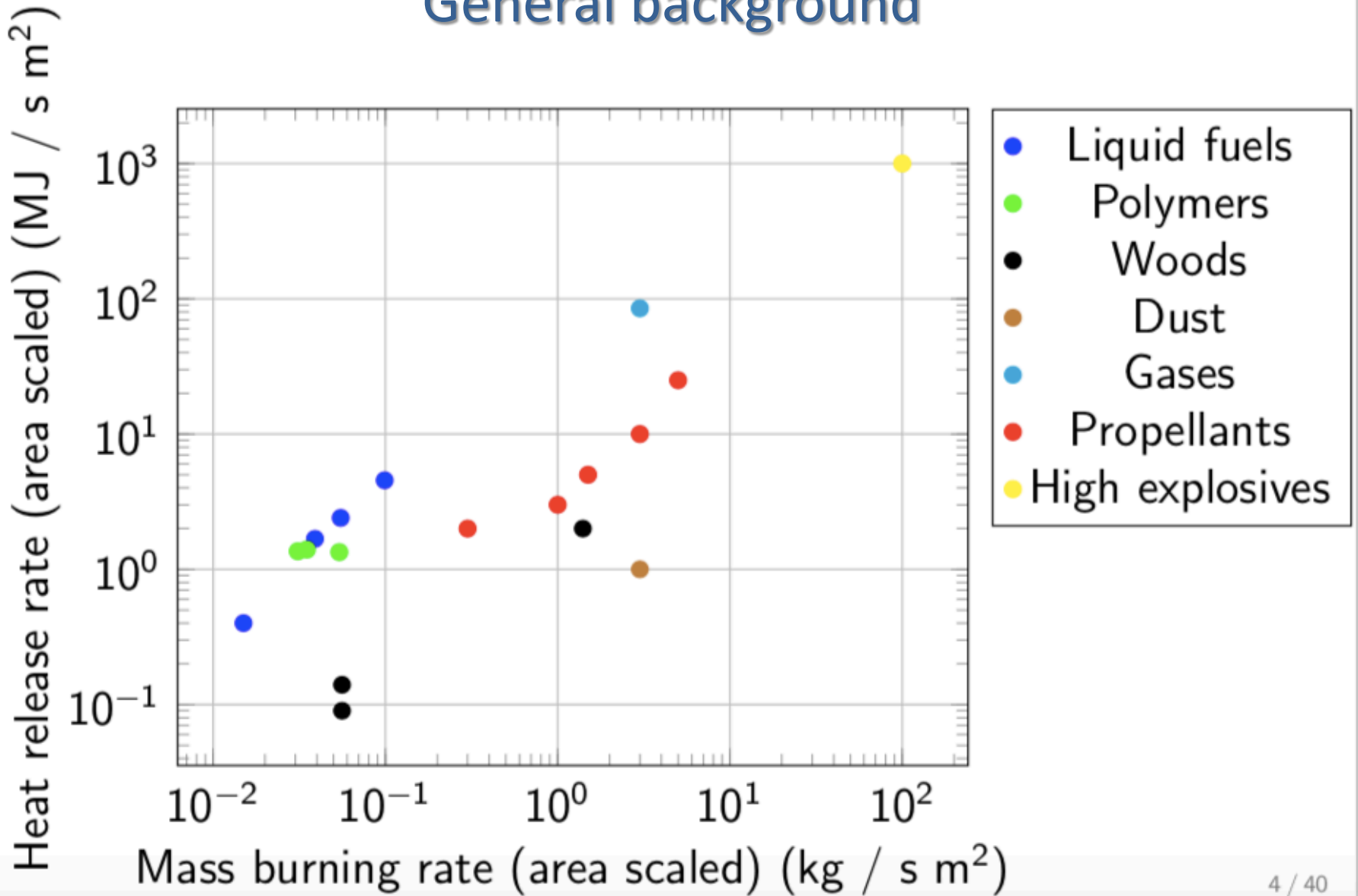
Since applications vary widely in their requirements, propellants can exhibit a large array of combustion behaviors.



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# Previous work

An attempt was made by Graham to model explosion venting and define a critical vent area ratio by equating pressure rise and decrease terms:

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A number of empirical relations have been published for gas and dust equations (see NFPA 68 for examples).

▶ Gas explosions:  $A_v = CA_s P_{red}^{-1/2}$

▶ Dust Explosions:  $A_v = 10^{-4} K_{st} V^{0.75} \left( \frac{P_{max}}{P_{red}} \right)^{1/2}$

→ Deflagration index,  $K_{st}$ , and reduced pressure,  $P_{red}$ .



# Theoretical background

Equation of state:

Nobel-Abel:

$$P(V - b) = NRT$$

when

$$X = cb \gg 0.01$$

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the ideal gas law:

$$PV = NRT$$



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Spatial pressure  
variation:

$$\chi = \frac{m_{air} c_{air}}{\dot{m}_{gen} d}$$

Lumped parameters

$$\rightarrow \chi \gg 1$$

Case	$\chi$ (dimensionless)
0.7 L closed vessel with a fast burning propellant	0.9
0.7 L closed vessel with a slow burning propellant	5.6
60 L tank with a fast burning propellant	420
1800 L enclosure with a fast burning propellant	561
10 <sup>6</sup> L enclosure with a fast burning propellant	675



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## Compressibility:

Studied pressures below 10 kPa

$$\rightarrow Ma < 0.30$$

Bernoulli's law:

$$v = \left( \frac{2P}{\rho_{gas}} \right)^{1/2}$$

Other cases:  
isentropic eq.



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$$\dot{m}_e + C_D A \left( \frac{2\rho_{gas} RT}{M_w V} \right)^{1/2} m_e^{1/2} - \dot{m}_{gen} = 0 \quad \text{when } 0 \leq t \leq t_{burn}$$



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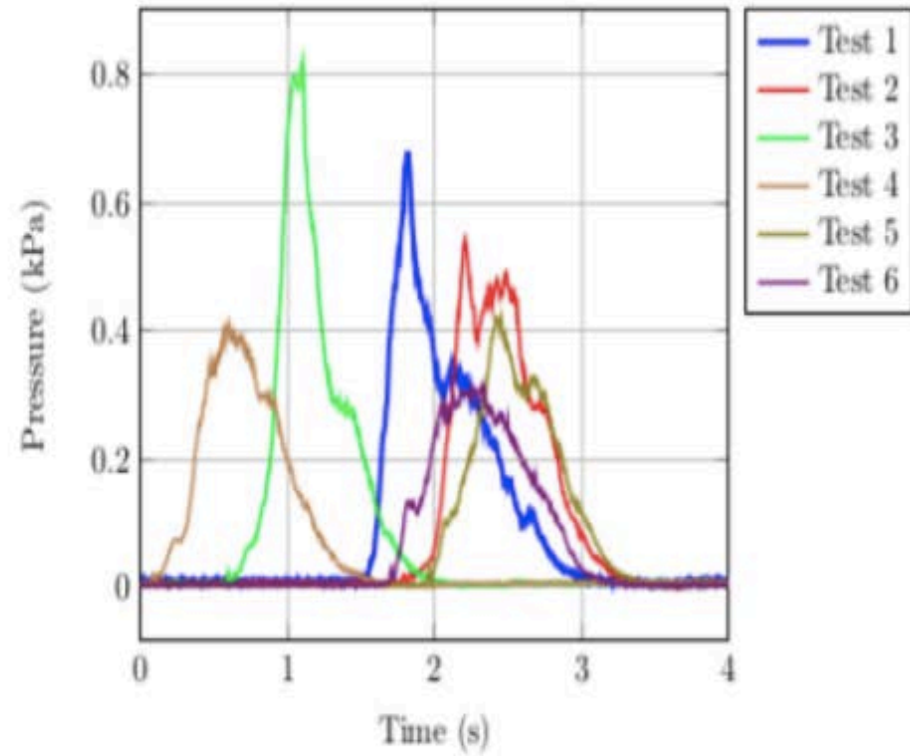




# Testing



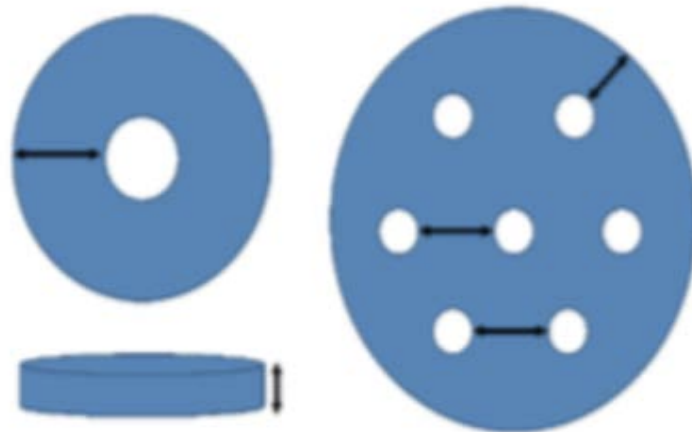
1800 L setup



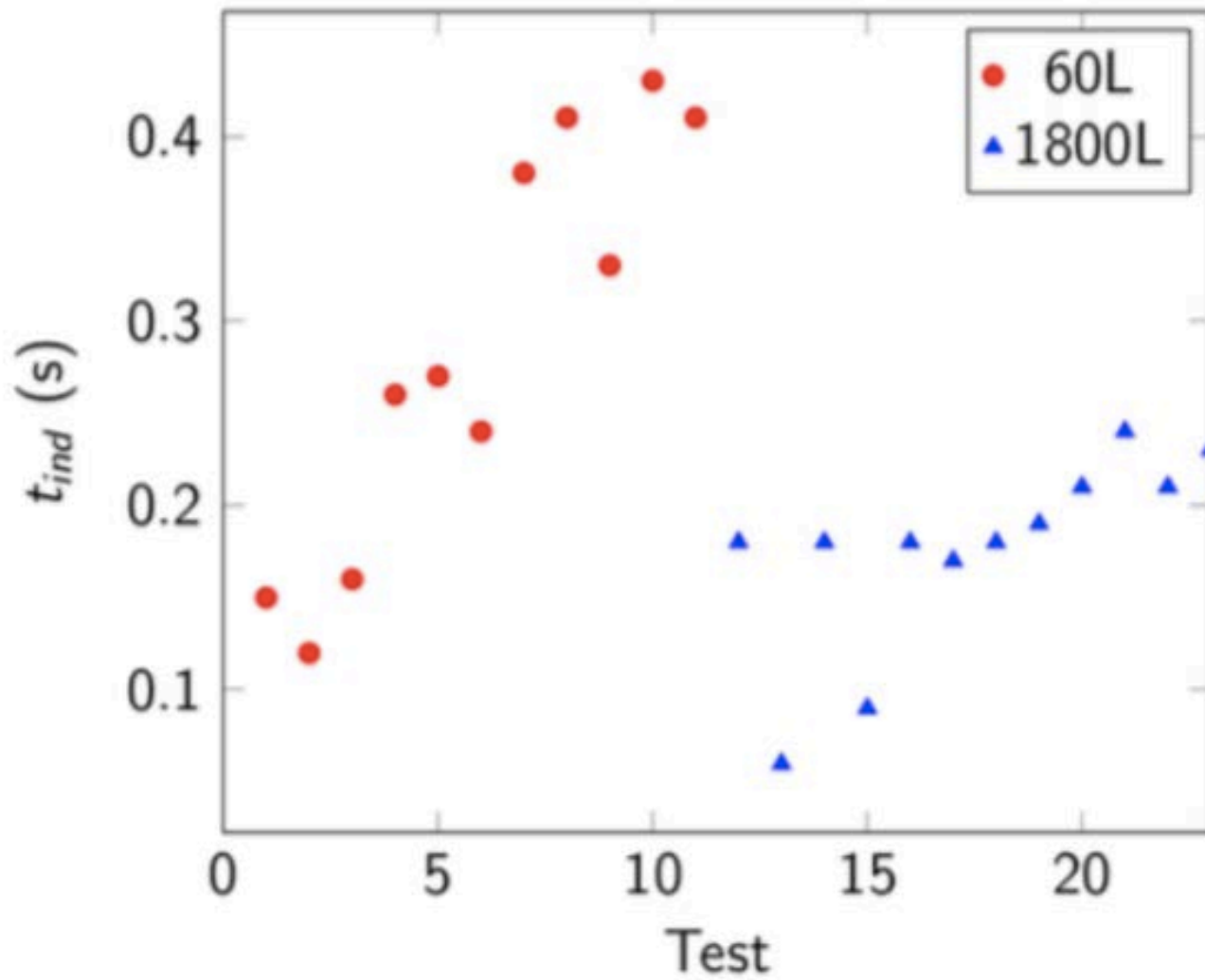
Typical measurement

# Testing

Propellant	Geometry	Heat of explosion (J/kg)	Composition
SB1	Unitubular	3871	NC: 98% / Inert: 2%
SB2	Unitubular	3135	NC: 90% / Inert: 10%
DB1	Cord	5392	NC: 60% / NG: 39% / Inert: 1%
DB2	Unitubular	4490	NC: 73% / NG: 25% / Inert: 2%

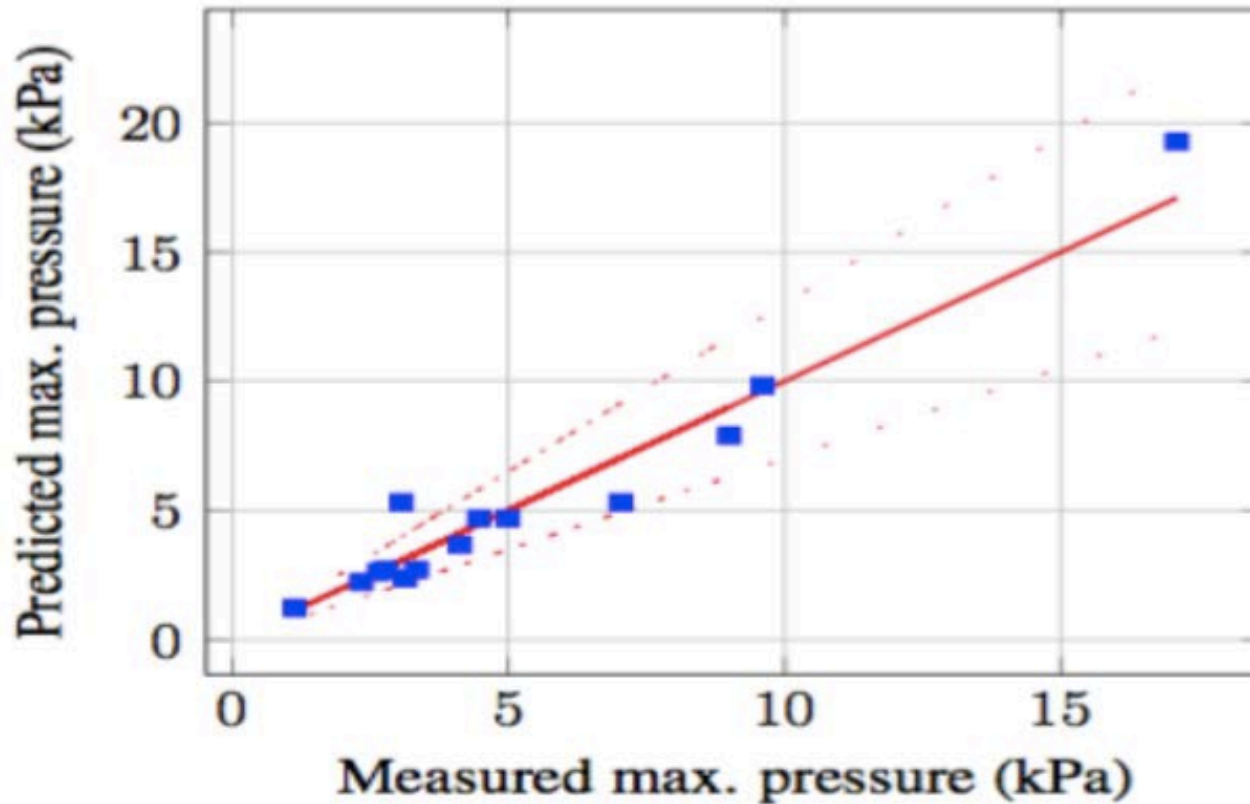


# Flame propagation – Induction time

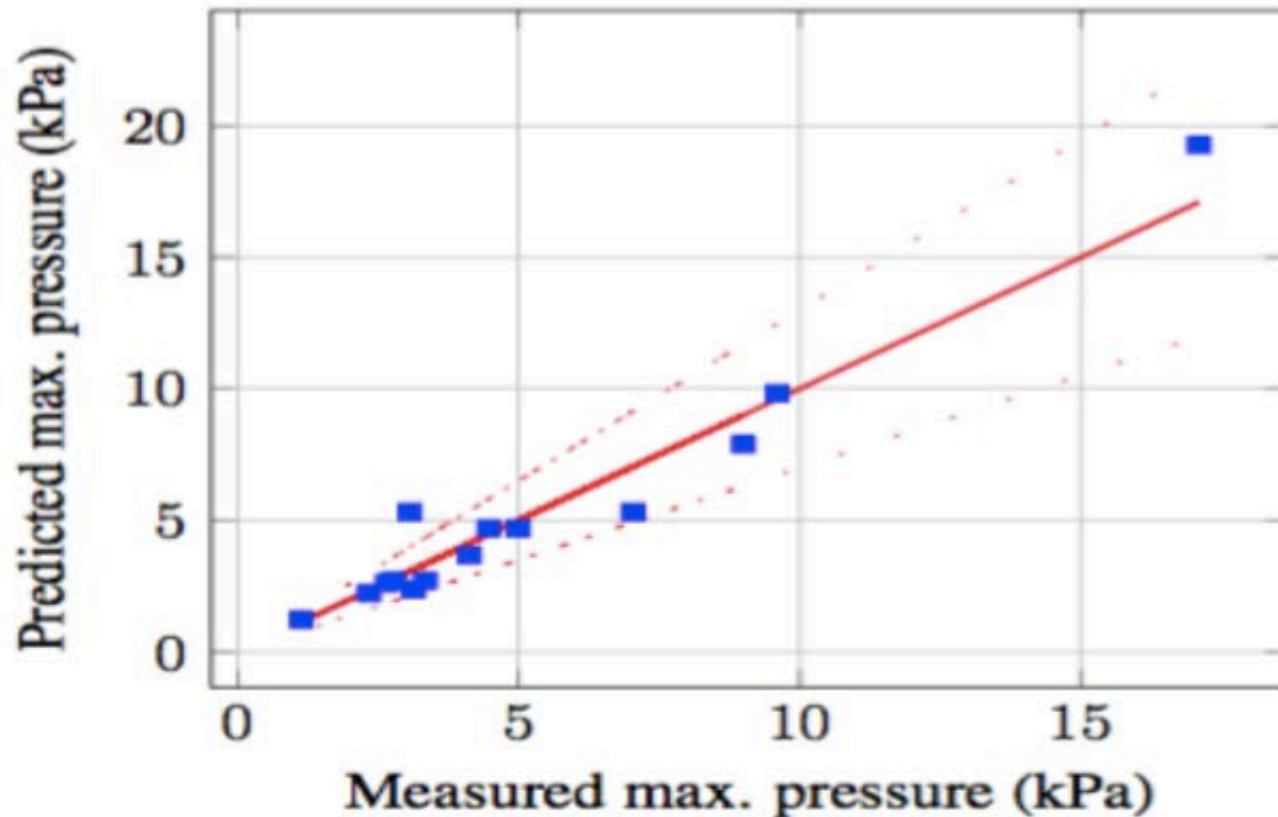


# Data analysis

Best statistical model:  $P_{max} = \frac{194.6m^{0.97}}{A^{1.34}}$  (with  $r^2 = 0.91$ )



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Departure from theoretical form suggests:  $C_D \approx A^{1/2}$

# Numerical model

Starting with the previously derived mass balance:

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An energy balance is also considered:

$$\Delta T = \frac{\dot{m}_{gen} E \Delta t - C_v \dot{m}_{vent} T \Delta t}{C_v (m_{air} + \rho_{gas} V)}$$



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Here, the mass generation rate can be approximated by:

$$\dot{m}_{gen} = \frac{m}{t_{max} - t_{ind}}$$



# Numerical model

Volume (m <sup>3</sup> )	Min. density (kg/m <sup>3</sup> )	Max. Temperature (K)
0.06	0.74	452
1.8	0.48	823
100	0.18	1798



# Numerical model

The gas density is estimated as

$$\rho_{gas} = 0.47 V^{-0.19}$$

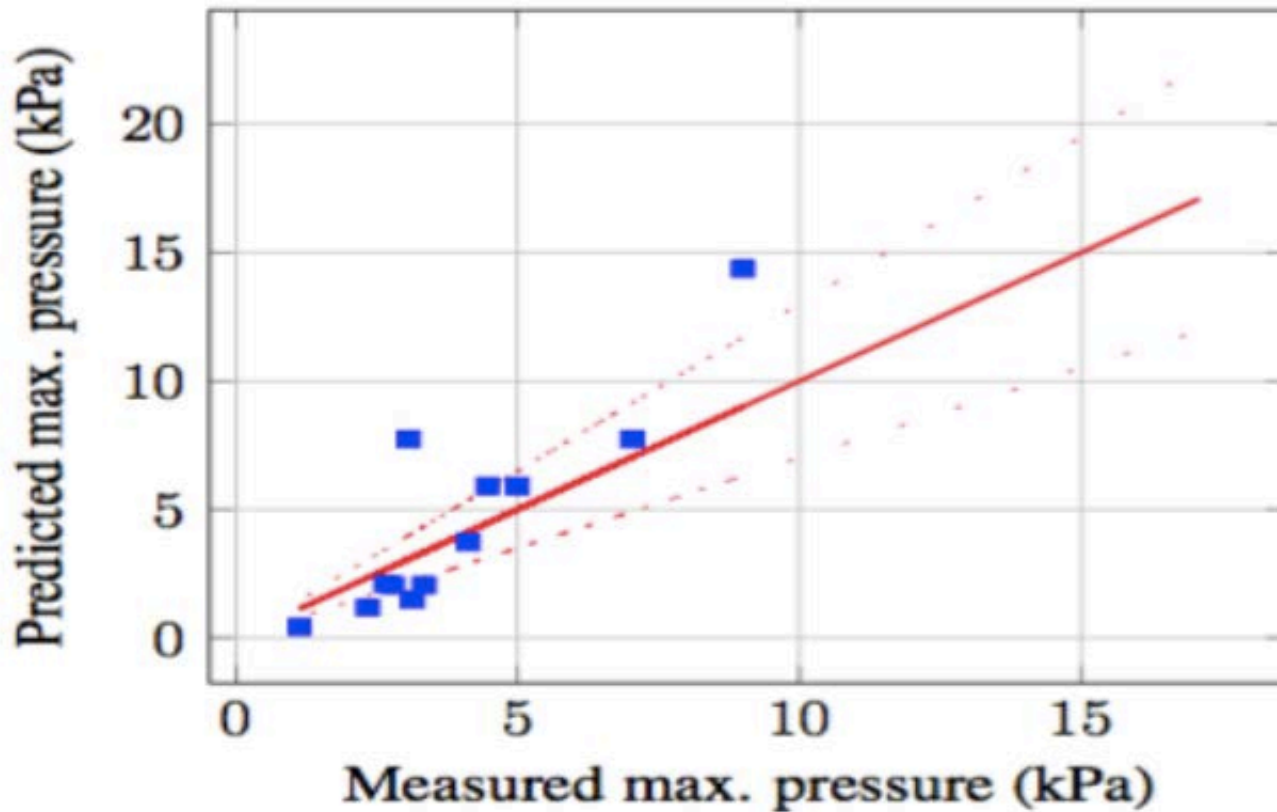
Subst. in theoretical model

$$\text{e.g. } P_{max} = \frac{1.06 m^2 V^{0.19}}{A^{2.66}}$$

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# Comparing the scale dependent model and measured results:



→ Loss in quality due to the uncertainty in estimating  $\dot{m}_{gen}$ .



# Future work

- Application to safety aspects
  - ▶ Quantities - distances relations, uniforms, building - process design, ...
- Better estimate of the mass combustion rate
- Application to “non dry” (or green) product
- Application to stick geometries (e.g. rocket motors)
- Application to cases at higher densities (higher pressures)



# Acknowledgements

- General Dynamics OTS Canada - Valleyfield
  - ▶ Use of their burning ground and equipments
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